

Fig. 1. Time dependence for the reduction of NaNO_3 (0.16 mol dm^{-3}) by AcrH_2 ($8.0 \times 10^{-4} \text{ mol dm}^{-3}$) in the presence of HClO_4 (1.0 mol dm^{-3}) in MeCN at 298 K. The calculated time dependence (\circ) is obtained by using Eq. 4. with $t_{1/2} = 159 \text{ s}$ and $c = 0.25 \text{ s}^{-1}$.

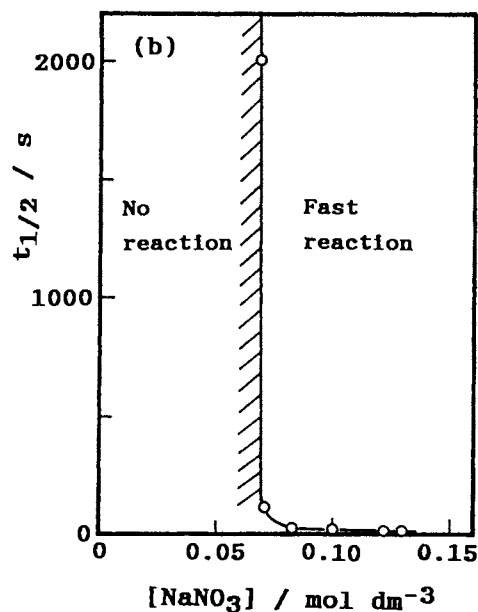
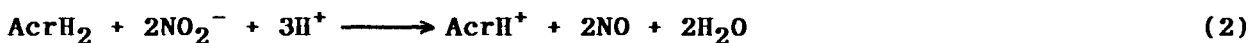


Fig. 2. Plot of the half-life ($t_{1/2}$) vs. $[\text{NaNO}_3]$ for the reduction of NaNO_3 by AcrH_2 ($5.0 \times 10^{-4} \text{ mol dm}^{-3}$) in the presence of HClO_4 (2.0 mol dm^{-3}) in MeCN at 298 K.

very slow rise in absorbance is followed by a rapid autocatalytic buildup of AcrH^+ . In such a case the half-life of the reaction ($t_{1/2}$) is approximately equal to the time when the rapid buildup starts. The $t_{1/2}$ value is extremely sensitive to the initial concentration of NO_3^- in the presence of excess HClO_4 . The dependence of $t_{1/2}$ on $[\text{NaNO}_3]$ in the presence of HClO_4 (2.0 mol dm^{-3}) is shown in Fig. 2, where a sharp dropoff of $t_{1/2}$ is observed at $[\text{NaNO}_3] > 7.0 \times 10^{-2} \text{ mol dm}^{-3}$. In the region $[\text{NaNO}_3] < 7.0 \times 10^{-2} \text{ mol dm}^{-3}$, no reaction has taken place at all. The value of such a critical concentration $[\text{NaNO}_3]_c$ is independent of $[\text{HClO}_4]$ which is in excess to $[\text{NaNO}_3]$. However, the $[\text{NaNO}_3]$ is very sensitive to the volume of the gas phase of the cuvette. As such no critical concentration of NaNO_3 has been observed, when the cuvette was filled with the reactant solution. The addition of a catalytic amount of NaNO_2 also causes the drastic decrease in the $t_{1/2}$ value.

We have recently reported that NO_2^- is readily reduced by AcrH_2 in the presence of HClO_4 in MeCN to yield NO and AcrH^+ (Eq. 2).⁶⁾ On the other



sudden buildup of AcrH^+ as shown in Fig. 1, demonstrating the validity of the kinetic formulation (Eq. 3).

If a tiny fraction of NO (α) is escaped from the solution to the gas phase (Scheme 1), Eq. 3 is rewritten by Eq. 5, where $[\text{AcrH}^+] = [\text{HNO}_2] +$

$$d[\text{AcrH}^+]/dt = [\text{AcrH}_2]\{k_1[\text{HNO}_3] + 2k_2([\text{AcrH}^+] - 3\alpha/2)\} \quad (5)$$

$(3/2)\alpha$. In such a case no rapid buildup of AcrH^+ may take place under the conditions that $[\text{HNO}_3] < (3k_2/k_1)\alpha$, since the rate of formation of AcrH^+ becomes zero when $[\text{AcrH}^+]$ reaches the value $(3/2)\alpha - (k_1/2k_2)[\text{HNO}_3]$. Under the conditions that $[\text{HNO}_3] > (3k_2/k_1)\alpha$, the reaction undergoes to completion.⁸⁾ This may be the reason why there exists the critical concentration of HNO_3 for the reaction as shown in Fig. 2, but why such a critical phenomenon disappears when the reaction cuvette is filled with the solution.

References

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- 5) The HNO_2 formed was separated from AcrH^+ by isolating as AgNO_2 by adding AgNO_3 to the resulting solution after neutralization with NaOH. Then, the yield of HNO_2 was determined by the absorption spectrum ($\lambda_{\text{max}} = 372$ nm, $\epsilon_{\text{max}} = 55.9 \text{ dm}^3 \text{ mol}^{-1} \text{ cm}^{-1}$).
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- 8) Only a trace amount of NO was detected in the gas phase of the cuvette by the glc analysis, indicating that $k_2 \gg k_1$.

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